



Full Length Article

Enhanced hydrogen evolution ability of Ru with regulation of interface electronic structure by WC/W₂C heterostructure via ultrafast flash joule heating synthesis

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ARTICLE INFO

Keywords:

Ruthenium
Tungsten carbide
Heterointerface
Hydrogen evolution reaction
Proton exchange membrane water electrolysis

ABSTRACT

Regulation of the electronic structure for ruthenium (Ru) based catalysts is critical but challenging to achieve highly active and stable performance at ampere-level current density for proton exchange membrane water electrolysis (PEMWE). In this work, two phase tungsten carbide heterostructure interface (WC/W₂C) is constructed to optimize adsorption of hydrogen intermediates (H*) on Ru-based heterostructure catalyst by one-step ultrafast flash joule heating. Experimental and theoretical studies indicate the obvious charge accumulation and migration at the interface region between Ru and WC/W₂C heterostructure. The H* adsorption and desorption balanced by tuning the interface electronic structure contributes synergistic effect to the HER activity of Ru-W_xC/CC. Accordingly, with a trace amount of Ru, the as-synthesized Ru-W_xC/CC exhibits an overpotential of 31 mV at 10 mA cm⁻² and 288 mV at 1 A cm⁻². Furthermore, the catalyst delivers exceptional stability during at least 500 h of operation at 10 mA cm⁻² with negligible degradation for overall water splitting. This work will provide a guidance for regulating interfacial electronic structure of hydrogen evolution catalyst by the design of heterostructure.

1. Introduction

Proton exchange membrane water electrolysis (PEMWE) can produce large-scale green hydrogen from renewable energy [1–4], due to its high energy efficiency, substantial current density, swift response time, and exceptional gas purity [5–8]. Where the highly efficient, low-cost, and stable catalysts for hydrogen evolution reaction (HER) play a significant role in promoting the performance of PEMWE devices. Platinum (Pt) is recognized as the state-of-the-art electrocatalyst toward HER, but its high cost and low reserves directly limit the large-scale application of PEMWE [9–13]. Over the past few decades, the catalytic activity of non-noble metal catalysts has significantly increased but is still not comparable with Pt/C due to their low intrinsic catalytic induced by the electronic structures [14–16].

Ruthenium (Ru), a relatively low-priced platinum-group metal with Pt-like metallic-H bond strength (65 kcal mol⁻¹), has garnered

considerable attention as a promising alternative [17–20]. Although Ru has potentially high HER activity, it is prone to agglomerate due to its larger cohesion energy than Pt [21]. Recent studies have designed uniform dispersion of Ru nanoparticles (NPs) [22], nanoclusters [23] and single-atom [24,25] catalysts. Uniformly dispersed Ru sites allow maximum utilization of metal species and increase efficiency. Additionally, the interaction between Ru and substrate has been proved to be crucial to regulate the surface physicochemical properties and electronic structure of Ru-based catalysts. The distinct hetero-interfacial effects occurring in the heterostructures can guide electronic reconstruction, binding energy optimization, active site enlargement, and electron transfer acceleration [26–28].

Metallic Ru-based heterostructure catalysts have attracted much attention in the field of electrocatalysis due to their excellent properties and the modification of electronic states at the heterogeneous interface [24]. Ren et al. designed Ru nanoclusters on carbon supports doped with

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<https://doi.org/10.1016/j.apsusc.2025.163015>

Received 4 January 2025; Received in revised form 20 February 2025; Accepted 17 March 2025

Available online 18 March 2025

0169-4332/© 2025 Published by Elsevier B.V.

controllable N-functional groups (NDC) carriers. The accumulation of electrons at the interface between the NDC carrier and Ru nanoclusters led to the asymmetric distribution of electrons, which promoted the adsorption and dissociation of water around the Ru sites [29]. In addition to the construction of heterogeneous structures with non-metallic carriers and single metallic Ru, there are also many studies on metal carbides/phosphates/sulfides/nitrides [30,31]. Metal carbides are widely used because of their excellent chemical and thermal stability, excellent corrosion resistance, and high electrical conductivity [32,33]. Specifically, metal carbide carriers promote the dispersion of metal atoms through strong electron interactions, triggering orbital hybridization and charge polarization at the interface to regulate catalytic activity [34,35]. In addition, metal carbide carriers combined with the potent H^* binding energy of Ru NPs will enhance the catalytic activity of HER significantly [36]. Li et al. constructed a β - Mo_2C -Ru nanoparticle heterogeneous catalyst. The interfacial interaction and strong electron coupling between Ru and Mo_2C optimized the adsorption/desorption of hydrogen intermediates and accelerated the acidic HER kinetics [37]. Jiang et al. realized efficient interfacial charge transfer by constructing lattice-matched Ru/ W_2C heterogeneous interfaces. The H^* adsorbed on the surface of W_2C rapidly migrated to the Ru site through the heterogeneous interface to reduce the hydrolytic dissociation barrier. Ru as a highly efficient H^* desorption site accelerated H-H coupling [38]. In summary, the activity of metallic Ru-based heterostructure catalysts is strongly dependent on a rich and highly active interface [24]. The two-phase heterostructure restricts the flexibility of adjustable characteristics of heterointerface. Accordingly, the design and construction of multi-phase heterostructure catalysts can open an avenue toward efficient heterostructure catalysts.

Herein, we constructed a Ru-based heterostructure catalyst by ultrafast flash joule heating. Ru NPs are uniformly dispersed on the

heterostructure of WC/W_2C . With a trace amount of Ru, the as-synthesized $Ru-W_xC/CC$ exhibits an overpotential of 31 mV at 10 mA cm^{-2} and 288 mV at 1 A cm^{-2} . Density functional theory reveals the obvious charge accumulation and migration at the interface region of $Ru-WC/W_2C$ heterostructure. The partial electrons transfer from Ru NPs to W_xC . The weakening of Ru-H bond promotes the desorption of H intermediate on Ru active sites. The ΔG_{H^*} of $Ru-W_xC/CC$ approaches to 0 eV, which can optimize hydrogen adsorption/desorption strength significantly and reduce HER reaction energy barrier. Furthermore, the catalyst delivers exceptional stability during at least 500 h of operation at 10 mA cm^{-2} with negligible degradation for overall water splitting.

2. Experimental section

Detailed information was given in [Supplementary Materials](#).

3. Results and discussion

3.1. Synthesis and characterizations of electrodes

In this work, the ultrafast flash joule heating technology was employed. Compared with traditional technology, this method can synthesize uniformly dispersed materials with remarkable steadiness swiftly in a short time. The structure and morphology of the catalyst can be controlled by changing the joule heating conditions [39–43]. Fig. 1a displayed the synthesis procedure of the $Ru-W_xC/CC$. Primarily, the carbon cloth (CC) substrate was treated in 65 % HNO_3 solution to increase surface hydrophilicity. Subsequently, the treated CC was immersed into 2 % polyethylenimine (PEI) solution to modulate the surface state of charge. PEI, characterized as a high C and N polymer, can shift the CC surface from negative charge state to positive charge

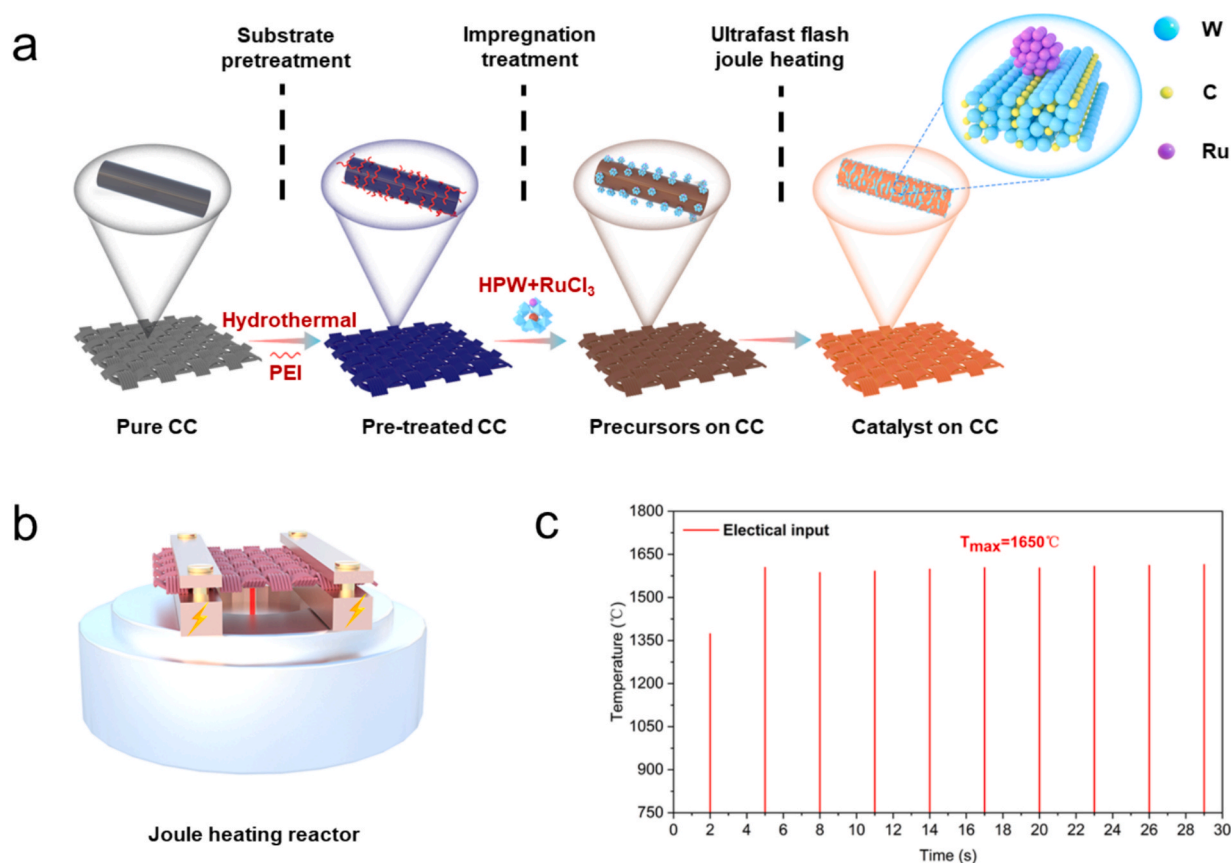


Fig. 1. a) Schematic illustration of the synthesis of $Ru-W_xC/CC$ by the ultrafast flash joule heating synthesis. b) Schematic diagram of the working condition of the joule heating reactor. c) A ten-pulse shock heating pattern demonstrates the uniform temperature in each cycle.

state [44,45]. For improving the dispersion of Ru NPs, the phosphotungstic acid anion (PW_{12}^{3-}) was chosen to adsorb and stabilize Ru^{3+} cations. The CC was impregnated into an ethanol solution containing $\text{PW}_{12}^{3-}/\text{Ru}^{3+}$ clusters. The $\text{PW}_{12}^{3-}/\text{Ru}^{3+}$ clusters with negative charge could be adsorbed on CC surface with positive charge [46,47]. Ultimately, the dry CC was rapidly heated to 1650°C for 100 ms by ultrafast flash joule heating in a vacuum atmosphere. Fig. 1b displayed the joule heating reaction device. In detail, two copper plates are used to fix the CC to form a conductive channel. The current flows through the CC via the conductive copper plate with a certain applied voltage. Due to joule heating effect, the CC carrier reaches the target temperature in a short time. Fig. 1c showed the temperature distribution during 10 joule heating pulse with 100 ms heating time. During calcination, the temperature was very stable. PW_{12}^{3-} was instantaneously pyrolyzed to form W_xC , and Ru^{3+} was reduced to metallic Ru [41,48,49]. Due to the pre-formed $\text{PW}_{12}^{3-}/\text{Ru}^{3+}$ cluster structure, the Ru NPs were uniformly dispersed and directly combined with the W_xC carrier to form heterostructures.

The scanning electron microscopy (SEM) images of the $\text{Ru-W}_x\text{C}/\text{CC}$, Ru/CC and $\text{W}_x\text{C}/\text{CC}$ were shown in Fig. 2a–b and Fig. S1. The $\text{Ru-W}_x\text{C}/\text{CC}$ exhibited the uniform nanoislands shape on the carbon fiber. The Ru/CC showed different morphology, and the spherical nanoparticles were distributed on the surface of the carbon fiber. The SEM images of the catalysts obtained with varying amounts of Ru and phosphotungstic acid (HPW) were shown in Figs. S2–3. The morphology of catalyst did not change too much with the loading of Ru and HPW. The SEM images of the catalysts obtained with varying amounts of the joule heating time and temperatures were shown in Figs. S4–5. With the increase of joule heating time, the size of catalyst increased obviously and the particles were agglomerated together. With the temperature increased, the particle size of the catalyst gradually became bigger. And at 1850°C , most of the particles were aggregated on the surface of the CC, which limited the mass transfer during the catalytic process and thus reduced the catalytic activity. The TEM of $\text{Ru-W}_x\text{C}/\text{CC}$ and $\text{W}_x\text{C}/\text{CC}$ at different resolutions were shown in Fig. 2c and Figs. S6–7. The high-resolution transmission electron microscopy (HRTEM) images confirmed the presence of Ru, WC, and W_2C three phases in Fig. 2d. The observed d-spacings of 0.173 nm, 0.259 nm, 0.203 nm corresponded to the (102) of W_2C , (100) of WC, and (002) of Ru, separately. The selected area

electron diffraction (SAED) pattern showed the diffraction patterns indexed to the (100) plane of WC, (102) plane of W_2C and (002) plane of Ru in Fig. 2e. The elemental mapping in Fig. 2f demonstrated that the $\text{Ru-W}_x\text{C}/\text{CC}$ was mainly composed of W, C and O elements, as well as a small amount of Ru (Fig. S8). Therefore, three-phase heterostructures were successfully constructed. For the $\text{W}_x\text{C}/\text{CC}$ in Fig. S9, the observed d-spacings of 0.250 nm, 0.172 nm corresponded to the (100) of WC and the (102) of W_2C , separately. The SAED pattern showed the diffraction patterns were indexed to the (100), (011) plane of WC and (002), (102) plane of W_2C . The element mapping diagram of the $\text{W}_x\text{C}/\text{CC}$ revealed the uniform distribution of W, O and C. ICP-MS was used to precisely quantitate the metal element amounts in $\text{Ru-W}_x\text{C}/\text{CC}$, as depicted in Table S1. The content of Ru was merely 1.44 wt%.

X-ray diffraction (XRD) was used to further confirm the crystal structure of the as-synthesized $\text{Ru-W}_x\text{C}/\text{CC}$, Ru/CC , $\text{W}_x\text{C}/\text{CC}$ and CC (Fig. 3a). In the $\text{Ru-W}_x\text{C}/\text{CC}$, the characteristic peaks at 31.51° , 35.64° and 48.29° are assigned to the (001), (100) and (101) planes of WC phase, the characteristic peaks at 34.53° , 39.59° and 43.23° are assigned to the (110), $(-1-11)$ and (102) planes of W_2C phase. This suggested the presence of two-phase W_xC NPs within the catalyst. The presence of three Ru diffraction peaks at 37.73° , 42.17° and 43.43° are assigned to the (100), (002) and (101) planes. The diffraction peaks of Ru were relatively weak, because of its ultralow content and well-distribution. This was consistent with the ICP-MS result. Similarly, the XRD result also proved that three-phase heterostructures were successfully constructed. Compared with $\text{W}_x\text{C}/\text{CC}$, introducing Ru into W_xC resulted in the diffraction peak intensity of Ru and W_xC diminished, and the phase content of WC/ W_2C phases changed. These findings aligned with those derived from both SEM and TEM characterization. Figs. S10–11 displayed the XRD results of catalysts with different concentrations of Ru and HPW. It was found that the position of the diffraction peak remained constant.

Raman spectrum was utilized to delve deeper into the structural details of $\text{Ru-W}_x\text{C}/\text{CC}$, $\text{W}_x\text{C}/\text{CC}$, and Ru/CC . In Fig. 3b, the peaks at 698 cm^{-1} and 861 cm^{-1} could be attributed to the W-C stretching mode, implying the formation of the W_xC phase [50]. The presence of a particular peak at 625 cm^{-1} might be related to the introduction of Ru, but the peak was very weak, possibly due to the minimal presence of Ru, indicating that Ru NPs were successfully introduced. In Fig. S12, D-band

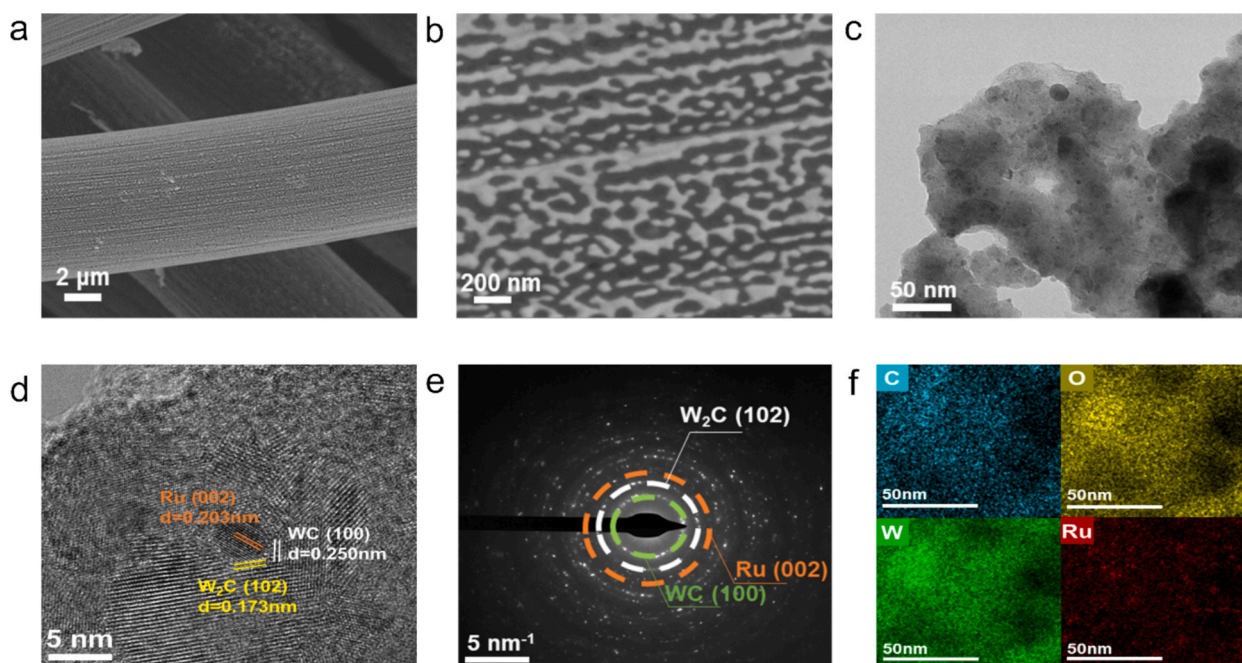


Fig. 2. a) and b) SEM images at different resolutions, c) TEM image, d) HRTEM image, e) SAED pattern f) EDS mapping diagram of $\text{Ru-W}_x\text{C}/\text{CC}$.

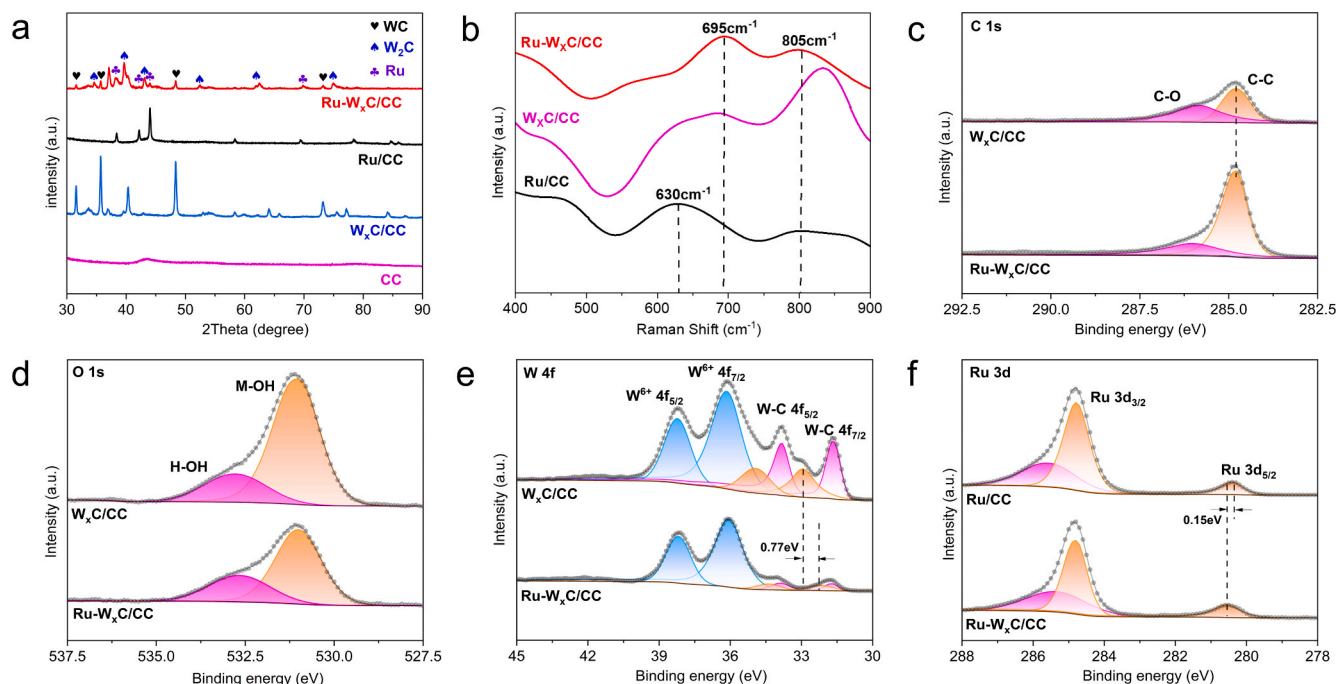


Fig. 3. a) XRD and b) Raman spectrum of Ru-W_xC/CC, W_xC/CC, and Ru/CC. c) C 1s, d) O 1s, e) W 4f and f) Ru 3d XPS spectra of Ru-W_xC/CC and W_xC/CC.

peak at 1350 cm⁻¹ corresponding to defective carbon and G-band peak at 1600 cm⁻¹ corresponding to graphitized carbon appeared. The I_G:I_D value of Ru-W_xC/CC was higher, indicating that Ru-W_xC/CC had higher conductivity, which was conducive to HER electrocatalytic hydrogen extraction performance [51,52].

X-ray photoelectron spectroscopy (XPS) was employed to gain a profound understanding of the valence state and distinctive electronic structure of the pristine Ru-W_xC/CC. The Ru, W, C and O elements could be clearly observed in the full-scan XPS survey spectrum of Ru-W_xC/CC (Fig. S13). There was no obvious signal of P and Cl elements in Ru-W_xC/CC, which was ascribed to the vaporization of the elements at high temperature. In the C 1s spectrum (Fig. 3c), the peaks at binding energy of 284.80 eV and 286.06 eV are assigned to C—C and C—O, respectively. Two characteristic peaks, namely hydroxyl group adsorbed on the surface of metal element (M—OH) (531.01 eV) and oxygen from adsorbed water (H—OH) (532.66 eV) on the surface of the material, could be observed in O 1s spectrum (Fig. 3d) [53]. The W 4f spectrum of Ru-W_xC/CC (Fig. 3e) could be deconvoluted into three pairs of characteristic peaks. Two strong peaks at binding energy of 36.06 eV and 38.19 eV are assigned to the W⁶⁺ 4f_{7/2} and W⁶⁺ 4f_{5/2} orbitals, respectively. Two strong peaks at binding energy of 31.71 eV and 33.88 eV are assigned to the W-C 4f_{7/2} and W-C 4f_{5/2} orbitals, respectively. They corresponded to W²⁺ valence states. Two satellite peaks at binding energy of 32.16 eV and 34.38 eV corresponded to W⁴⁺ valence states [54]. The presence of W⁶⁺ might stem from surface oxidation, which in turn enhanced the W⁴⁺ valence. Compared with W_xC/CC, the lower proportion for high valence W⁶⁺ peak in Ru-W_xC/CC indicated that the surface oxidation degree of Ru-W_xC/CC was lower than that of W_xC/CC [55]. The ratio of W⁴⁺ and W²⁺ peak areas in Ru-W_xC/CC was approximately 1:1, indicating the presence of a mixture of WC and W₂C phases. However, the signal intensity and ratio of W⁴⁺ and W²⁺ in W_xC/CC were significantly stronger than that in Ru-W_xC/CC. The content of high valence W⁴⁺ might adsorb hydrogen intermediate (H*) through stronger W-H bond in HER reaction, but too strong adsorption could lead to desorption difficulty and inhibit HER kinetics [56,57]. Proper ratio of W⁴⁺ to W²⁺ could optimize the adsorption/desorption equilibrium of H* and increase the activity of HER. The binding energy of W⁴⁺ within Ru-W_xC/CC negatively shifted to lower binding energy compared with W_xC/CC which

indicated electrons were transferred between W₂C and WC. This proved that abundant electron transfer from W₂C to WC through two-phase interface. In the Ru 3d spectrum of Ru-W_xC/CC (Fig. 3f), the peaks at binding energy of 284.79 eV and 280.55 eV are assigned to Ru 3d_{3/2} and Ru 3d_{5/2} of metallic Ru, respectively, and the one weak peak at binding energy of 285.4 eV is assigned to oxidized Ru species [4]. The binding energy of metallic Ru⁰ species gradually moved to the higher binding energy direction relative to the Ru/CC contrast sample, indicating that the introduction of Ru led to partial electrons transport from Ru NPs to W_xC. The above XPS results demonstrated that there was charge transfer between Ru and W_xC, and strong electronic coupling around the three-phase heterogeneous interface, which could effectively regulate the electronic structure of Ru.

3.2. Electrochemical measurement of HER activities

The HER activity of Ru-W_xC/CC, W_xC/CC, Ru/CC and commercial Pt/C were evaluated in 0.5 M H₂SO₄ using a three-electrode system. The content of Ru and HPW were optimized, as shown in Fig. S14-15. When the mas loading of Ru and HPW were 0.56 mg cm⁻² and 4 mg cm⁻² respectively, the catalyst possessed optimal HER activity. In Fig. 4a, the LSV polarization curve showed that the overpotential of Ru-W_xC/CC was 31 mV at 10 mA cm⁻² current density. The activity was comparable to that of the commercially available 20 % Pt/C catalyst (0.5 mg cm⁻² loading). For comparison, the W_xC/CC delivered an overpotential of 218 mV and Ru/CC with the identical Ru loading had an overpotential of 67 mV, which illustrated that Ru site was dominated in the HER activity and required to be regulated. Additionally, Ru-W_xC/CC enabled to operate at 1 A cm⁻² current density with an overpotential of 288 mV. The activity enhancement of Ru-W_xC/CC was mainly derived from the regulation effect of WC/W₂C heterostructures on Ru electronic structure.

The Tafel curves were fitted from the LSV curve to distinguish the HER mechanism in Fig. 4b. For the W_xC/CC, the Tafel slope reached 70 mV/dec, indicating that the Volmer step of proton adsorption on the catalyst surface was the Rate-Determining Step (RDS). After the integration of Ru, the Tafel slope dropped to 43.15 mV dec⁻¹, which was close to the theoretical value of the Heyrovsky step (40 mV dec⁻¹),

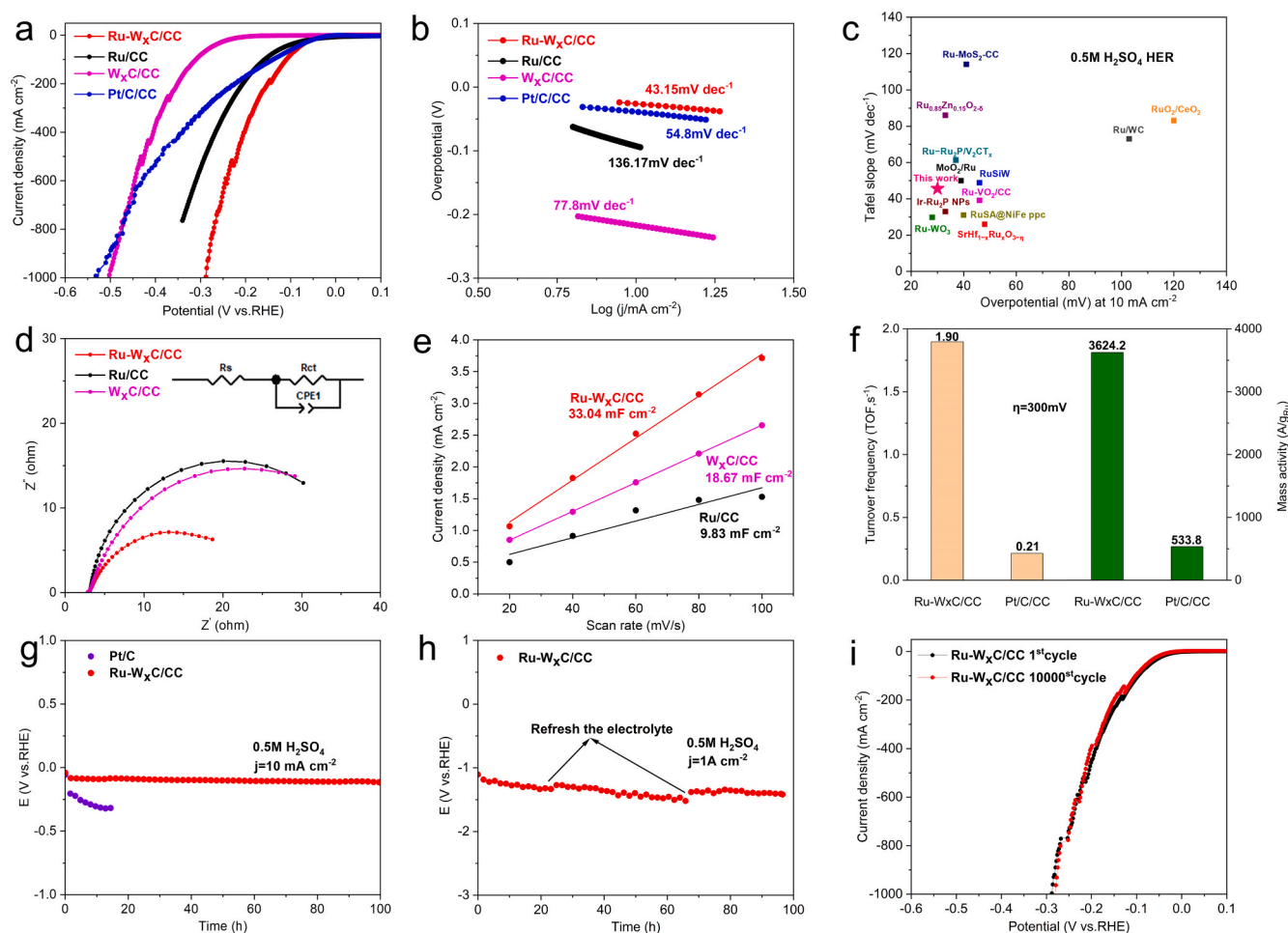


Fig. 4. a) LSV curves of Ru-W_xC/CC, Ru/CC, W_xC/CC and 20 % Pt/C/CC in 0.5 M H₂SO₄. b) Tafel curves of Ru-W_xC/CC, Ru/CC, W_xC/CC in 0.5 M H₂SO₄. c) Comparison of the activity of Ru-based hydrogen evolution catalysts. d) EIS curves, e) C_{dl} curves of Ru-W_xC/CC, Ru/CC, W_xC/CC. f) Comparison of TOF and Mass activity values of Ru-W_xC/CC and 20 % Pt/C/CC when $\eta = 300$ mV. g) Stability comparison at 10 mA cm⁻² of Ru-W_xC/CC and 20 % Pt/C/CC. h) Stability of Ru-W_xC/CC at 1 A cm⁻². i) Ru-W_xC/CC acceleration stress curve.

indicating more rapid HER kinetics. The HER occurred via the Volmer-Heyrovsky mechanism. The overpotential and Tafel slope of the Ru-W_xC/CC at 10 mA cm⁻² were compared with the reported Ru-based hydrogen evolution catalysts (Fig. 4c), and the results showed that the kinetics were better than most reported catalysts. The decreased slope suggested that the adsorption/desorption strength of H intermediates on the Ru-W_xC/CC had been optimized via a synergistic effect between Ru and WC/W₂C heterostructures.

Electrochemical impedance spectroscopy (EIS) measurements were conducted to profoundly investigate the outstanding HER activities of the Ru-W_xC/CC. The fitted Nyquist plots in Fig. 4d showed the charge transfer resistance of Ru-W_xC/CC (10.3 Ω) is much lower than that of W_xC/CC (20 Ω) and Ru/CC (17.2 Ω) in 0.5 M H₂SO₄ solution, confirming that the catalyst exhibited fast electron transfer capability toward the HER.

The specific surface area of the electrochemical activity of catalysts is one of the important factors to affect the catalytic activity of catalysts. The cyclic voltammetry (CV) curve of the catalysts in the non-Faraday region was measured in 0.5 M H₂SO₄ solution by different scan rates. The CV curves with different Ru and HPW contents were shown in Fig. S16–17. The CV curve was fitted to obtain the correlation curve with current density at different sweeping rates, and the slope was calculated to obtain the capacitance value of the electrochemical double-layer capacitance (C_{dl}) (Fig. 4e). The Ru-W_xC/CC had a higher double layer capacitance of 33.04 mF cm⁻², while W_xC/CC and Ru/CC had a double

layer capacitance of 18.67 mF cm⁻² and 9.83 mF cm⁻², respectively. The C_{dl} with different Ru and HPW contents were shown in Fig. S18. The electrochemical surface area (ECSA) was normalized from LSV curves (Fig. S19). The ECSA of Ru-W_xC/CC was 944 cm² which was much higher than that of W_xC/CC, which illustrated that Ru-W_xC/CC exhibited the higher intrinsic activity than W_xC/CC. Therefore, the HER activity of the catalyst was essentially enhanced.

The Ru clusters in Ru-W_xC/CC with high surface-to-volume provided highly exposed active sites to significantly improve the metal utilization efficiency of Ru. As shown in Fig. 4f. When the overpotential was 300 mV, the mass activity of the catalyst was 3624.2 A g⁻¹ and the TOF value was 1.9 s⁻¹, surpassing commercial Pt/C by 6.8- and 9- fold, respectively.

The long-term stability of the Ru-W_xC/CC was further estimated by chronopotentiometry (CP) test in 0.5 M H₂SO₄ solution. In Fig. 4g, the Ru-W_xC/CC exhibited long-term stability for over 100 h at 10 mA cm⁻², whereas Pt/C only operated 10 h. The Ru-W_xC/CC also operated stably for more than 100 h at 500 mA cm⁻² and 1 A cm⁻² in Fig. 4h and Fig. S20. The overpotential decayed at the rate of 0.3 mV/h. In parallel, the polarization curve of Ru-W_xC/CC (Fig. 4i) exhibited insignificant performance deterioration. The overpotential declined about 5 mV at 10 mA cm⁻² after 10,000 continuous CV cycles at the scan rate of 100 mV/s, suggesting its satisfactory durability under acidic condition. Subsequently, we analyzed the crystal structure before and after HER by XRD in Fig. S21. The XRD pattern showed that the position of the peak

did not change after the XRD test, indicating that the crystal structure after HER remained intact. We also analyzed the chemical states of C, O, Ru, and W in Ru-W_xC/CC after HER by XPS in Fig. S22. The C 1 s spectrum showed that C occurred a certain degree of oxidation. The O 1 s spectrum showed that the content of oxygen from adsorbed water is significantly increased. The Ru 3d spectrum showed that the metallic Ru⁰ disappeared near 280 cm⁻¹, indicating a slight dissolution of Ru species. The W 4f spectrum after the test showed that the low state peak of W disappeared, which proved that W occurred a slight oxidation.

The overall water splitting was evaluated in 0.5 M H₂SO₄ by directly using Ru-W_xC/CC as cathode and RuWO_x/CC as anode in Fig. 5a. The preparation of RuWO_x/CC was indicated in the experimental details. In contrast to the preparation of Ru, it was sintered directly in the air. As a comparison, 20 % Pt/C and RuWO_x/CC were adopted as cathode and anode, respectively. In Fig. 5b, the Ru-W_xC/CC || RuWO_x/CC cell showed a cell voltage of 2.09 V @1000 mA cm⁻² which was higher than the Pt/C || RuWO_x/CC cell. As shown in Fig. 5c, The Ru-W_xC/CC || RuWO_x/CC cell showed higher stability. After CP tested up to at least 500 h @10 mA cm⁻², the voltage of Ru-W_xC/CC || RuWO_x/CC cell had only 100 mV voltage increase. The voltage maintained the initial values of 99.3 % after 500 h operation. While the Pt/C || RuWO_x/CC cell only operated for 275 h before it completely lost its full activity. Therefore, The Ru-W_xC/CC was suitable for commercial use and meets the requirements of actual working conditions because of its excellent overall water splitting activity.

3.3. Mechanism for the enhancement of HER in acid

To further reveal the adsorption behavior of hydrogen on the catalyst surface during HER, in-situ Raman spectrum were conducted in acidic media (Fig. S23). The voltage range was selected from -0.4~0.2 V (relative to the reversible hydrogen electrode (RHE)), including the non-Faraday region and HER hydrogen evolution region. At a specific potential of 0.1 V (vs. RHE), the surface of catalyst began to adsorb the hydrogen protons. A new peak appeared near 2325 cm⁻¹, which might be attributed to the result of Ru-H stretching vibration. The intensity of this peak further rose with increasing the applied cathodic potential. In this process, the rate-determining step (RDS) changed from the Volmer step to the Heyrovsky or Tafel step. Therefore, the H on Ru was a reaction intermediate in the HER, and the Ru-H bond was an important factor in determining HER activity [58,59]. Similarly, in infrared spectrum (Fig. S24), there was no significant change before impregnation. After impregnation, the absorption peak in the range of 600~1000 cm⁻¹ associated with W-O stretching modes. After carbonization, the absorption peak in the range of 600~800 cm⁻¹ associated with W-C stretching modes. After the HER hydrogen evolution test, the peaks in the range of 1500~2000 cm⁻¹ related to the formation of the Ru-H bond, whereas the peaks near 1200 cm⁻¹ associated with the formation of the W-H bond. The above results showed that W and Ru were bonded to H during the HER process.

The superior catalytic performance of the Ru-W_xC/CC was further

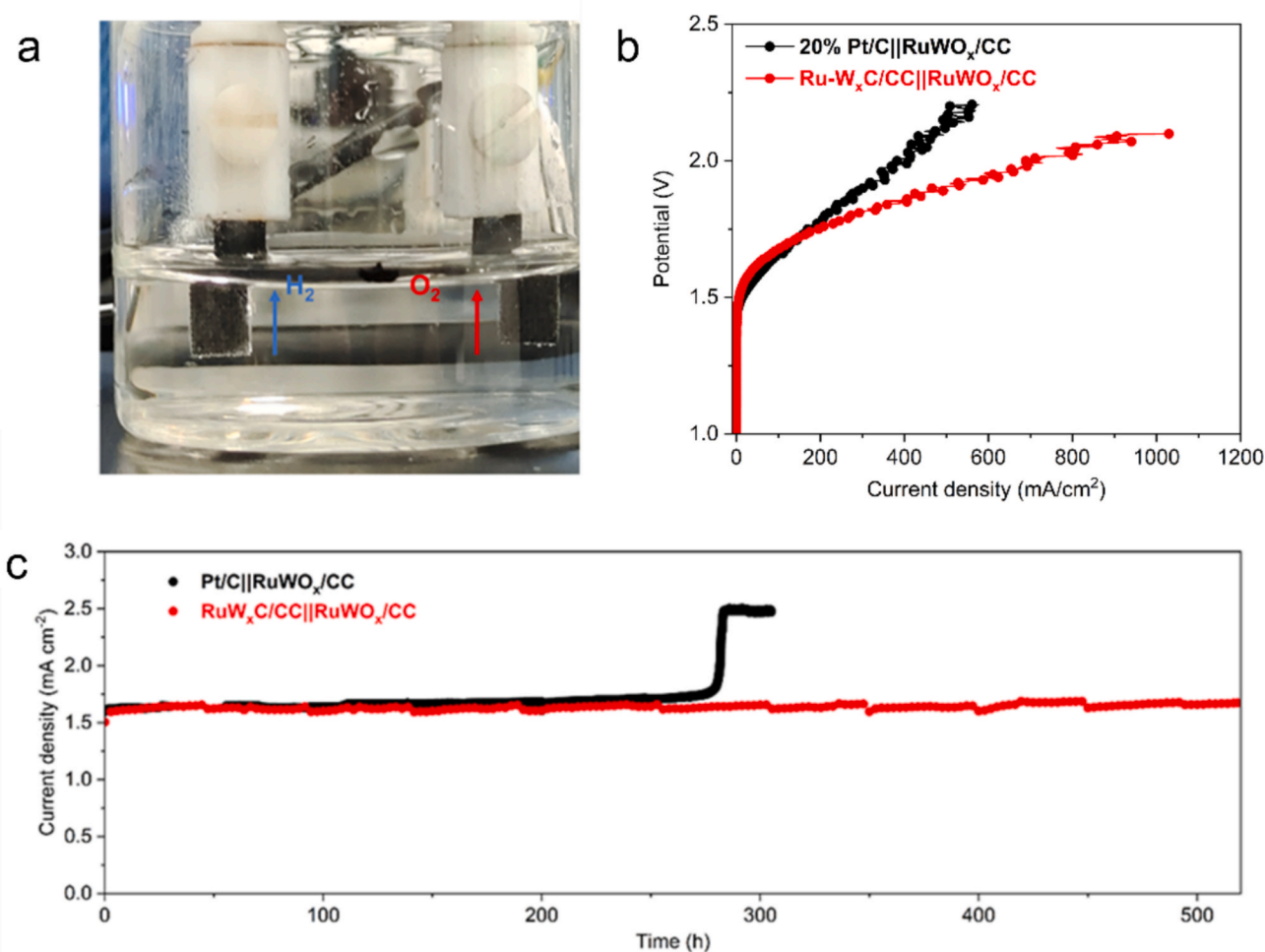


Fig. 5. a) Laboratory test diagram of overall water splitting in double electrode system. b) LSV comparison diagram of Ru-W_xC/CC || RuWO_x/CC and Pt/C || RuWO_x/CC. c) Stability test diagram of Ru-W_xC/CC || RuWO_x/CC at 10 mA cm⁻².

verified by density functional theory (DFT) [60]. To simulate the corresponding HER activity, the HER mechanism in acid consisting of the following three steps was considered, where the asterisk (*) indicated a certain surface species or an empty site [61–64]:

- 1) Volmer reaction: $\text{H}^+ + \text{M} + \text{e}^- \rightarrow \text{MH}^*$
- 2) Heyrovsky reaction: $\text{MH}^* + \text{H}^+ + \text{e}^- \rightarrow \text{M} + \text{H}_2$
- 3) Tafel reaction: $2\text{MH}^* \rightarrow 2\text{M} + \text{H}_2$

The HER mechanism includes the Volmer-Heyrovsky or Volmer-Tafel pathway. Both pathways are involved in the formation of H^* , and ΔG_{H^*} is an important index for predicting the activity of HER catalysts. This index is related to the electronic structure and surface chemistry of the catalysts. For an ideal catalytic site for the HER, the ΔG_{H^*} should approach to zero. Based on the TEM results, we constructed three catalyst models of Ru (002), two-phase heterostructure WC (100)/W₂C (102) and Ru (002)-WC (100)/W₂C (102), respectively (Figs. S25–27, Fig. 6a). To explore the optimized electronic structure of Ru around heterointerface, electron density difference at the interface region was plotted in Fig. 6b. It was found that the obvious electron accumulation and charge transfer at the heterostructure interface. HER activity was improved by regulating the electronic structure and optimizing binding energy through the heterostructure interface effect. The Bader charge diagram of WC (100)/W₂C (102) was shown in Fig. S28, and obvious

electron accumulation and migration could also be found at the interface of the two-phase heterostructure. The charge transfer quantities of Ru, WC, and W₂C in Ru-W_xC/CC and W_xC/CC were shown in Table S2. The Bader charge value of Ru (002) was positive, indicating that there was an outflow of charge. Compared with W_xC/CC, the decrease of Bader charge value of WC (100) in Ru-W_xC/CC indicated that a large amount of charge transferred from W₂C to WC. These results were consistent with the XPS results. Ru NPs in Ru-W_xC/CC (−0.35 |e|) exhibited a charge close to the metallic state in Fig. 6c. According to the partial density of states (PDOS) plots in Fig. 6d. The d-band center value of Ru-WC/W₂C (Ru) was −2.94 eV. It was 0.03 eV lower than that of Ru (Ru), which indicated that the electron coupling between Ru and W atoms reduced the charge transfer resistance. According to the d-band theory, the downshift of the d-band center signified that the adsorption between Ru and reaction intermediates was weakened, which promotes the process of desorption. Ru-WC/W₂C (Ru) had a higher electron density near the fermi level, which facilitated the adsorption of H intermediates. Similarly, a similar conclusion could be obtained from the change of d-band center value at the W site. As a result, the adsorption/desorption of hydrogen intermediates was optimized. As revealed by Tafel slope results, the HER process of Ru-W_xC/CC in acidic environments followed a Volmer-Heyrovsky pathway, in which the reaction involved H₂O adsorption, H₂O dissociation, the formation of H^* intermediates and H₂. The dissociation energy barrier diagram of water was shown in Fig. 6e.

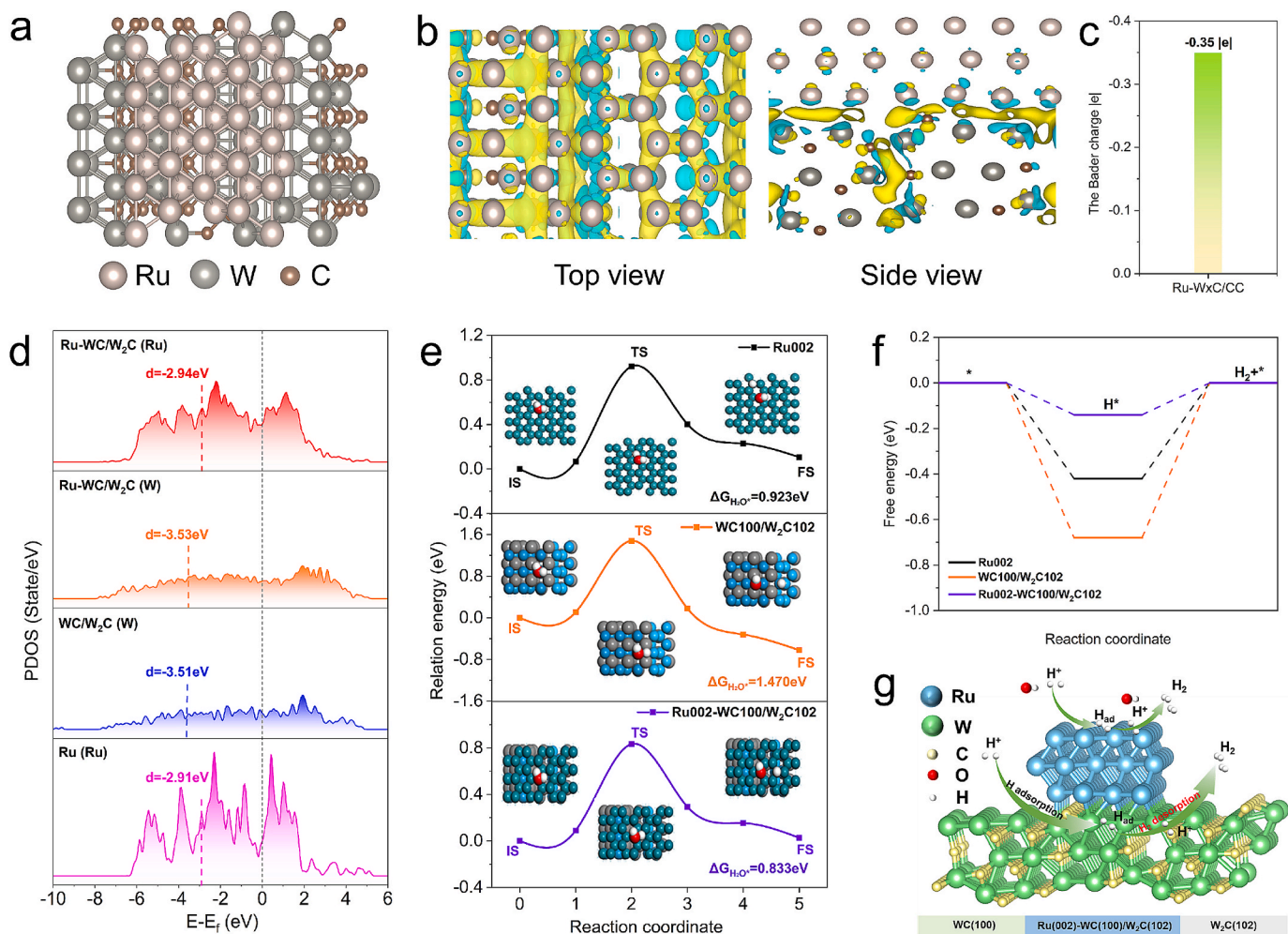


Fig. 6. a) Ru (002)-WC (100)/W₂C (102) calculation model diagram. b) Differential charge density of Ru-W_xC/CC. c) Bader charge analysis of Ru-W_xC/CC. d) The PDOS plots of Ru-W_xC/CC (Ru), Ru-W_xC/CC (W), W_xC/CC (W) and Ru (Ru). e) Dissociation energy barrier diagram of water and f) Hydrogen adsorption energy barrier diagram on Ru-W_xC/CC, W_xC/CC and Ru. g) Schematic illustration of heterointerface synergy between Ru, WC and W₂C for enhanced HER under few proton conditions.

The $\Delta G_{H_2O^*}$ of Ru-WC/W₂C was 0.833 eV lower than Ru ($\Delta G_{H_2O^*} = 0.923$ eV) and WC/W₂C ($\Delta G_{H_2O^*} = 1.47$ eV), indicating that water was more easily dissociated in Ru-WC/W₂C. As shown in Fig. 6f, Ru-WC/W₂C had a lower hydrogen adsorption energy barrier ($\Delta G_{H^*} = -0.14$ eV), which was closer to zero than Ru ($\Delta G_{H^*} = -0.42$ eV) and WC/W₂C ($\Delta G_{H^*} = -0.68$ eV). This indicated that the introduction of Ru and more heterostructure interface could effectively promote the adsorption/desorption of hydrogen intermediates, thereby improving HER activity. This was consistent with the results of PDOS.

The elevated HER activity and stability of Ru-WC/W₂C in acidic media are related to the following aspects: Primarily, the strong electron coupling occurs at the Ru/W_xC and WC/W₂C two-phase heterostructure, which optimizes the electronic structure of Ru and W active sites, reduces the energy barrier of the reaction process and accelerates HER kinetics. This enhances the catalytic ability of the active site which facilitates the process of hydrogen desorption and water dissociation in acidic media. Fig. 6g showed two hydrogen evolution pathways. The H generated by hydrolysis is directly adsorbed on Ru interface or adsorbed at the three-phase heterogeneous interface to generate H*, then the H* combines with H ion derived from another H₂O molecule to form H₂. Furthermore, the uniform distribution of Ru-WC/W₂C NPs on the carbon carrier is not only conducive to the exposure of the active site and the acceleration of electron transfer but also conducive to the mass transfer of gas products, allowing for rapid separation of bubbles formed by high current density [51]. Thus, the high activity of the catalyst in acidic media and the highly durable HER performance in long-term operation are guaranteed.

4. Conclusion

In summary, Ru-W_xC/CC heterostructure is successfully developed by the ultrafast flash joule heating route. Ru NPs are uniformly dispersed on the heterointerface of WC/W₂C. DFT calculations demonstrate that the electronic interaction between Ru and W_xC optimizes the adsorption/desorption of H intermediates and the dissociation of H₂O. Their synergistic effect yields excellent activity for HER in acidic media, only exhibiting a low overpotential of 31 mV at 10 mA/cm², and 288 mV at 1 A/cm². The catalyst delivers a remarkable durability at least 500 h (at 10 mA cm⁻²) for overall water splitting. This work not only provides a fast and efficient alternative for the synthesis of catalysts with excellent activity and stability but also provides guidance recommendations for the continued exploration of designing efficient electrocatalysts.

CRediT authorship contribution statement

Yongkang Liu: Methodology, Investigation, Formal analysis, Data curation. **Fulai Qi:** Writing – review & editing, Supervision, Investigation, Funding acquisition, Conceptualization. **Xinqiang Wang:** Investigation, Funding acquisition. **Qian Zhang:** Formal analysis, Data curation. **Yanxia Liu:** Methodology, Funding acquisition. **Yong Gao:** Software, Formal analysis. **Ke Wang:** Methodology, Formal analysis. **Wengang Cui:** Software, Methodology. **Fan Gao:** Methodology, Formal analysis. **Zhenglong Li:** Software, Formal analysis. **Yaxiong Yang:** Writing – review & editing, Formal analysis. **Lixian Sun:** Writing – review & editing, Supervision, Funding acquisition. **Jian Chen:** Writing – review & editing, Supervision, Funding acquisition. **Hongge Pan:** Writing – review & editing, Supervision, Funding acquisition, Conceptualization.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Acknowledgements

The research was supported by the National Natural Science Foundation of China (Nos. 52301287 and 52201275), the Scientific Research Program Funded by Education Department of Shaanxi Provincial Government (No. 23JK0490), the Natural Science Foundation of Shaanxi Province (No. 2023-JC-QN-0470) the Major Special Project of the Integration of Two Chains for the Qin Chuangyuan Construction (No. 23LLRHZDX0017), and the Foundation of Guangxi Key Laboratory of Information Materials (No. 221005-K).

Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.apsusc.2025.163015>.

Data availability

Data will be made available on request.

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